

## DETERMINATION OF TEMPERATURE AT DIFFERENT LOCATIONS OF THE QUARTZ VIAL CONTAINING 40 GM OF $\text{TeO}_2$ DURING ITS IRRADIATION IN THE DCT AT 3MW OF BAEC TRIGA MK-II RESEARCH REACTOR

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### ABSTRACT

The study is done to analyze particularly the temperature of the quartz vial wall and also the temperature in and around the sample that contained 40 gm of  $\text{TeO}_2$  powder using one dimensional analysis technique. The sample was irradiated with the help of thermal neutron flux  $8.71 \times 10^{13}$  n/cm<sup>2</sup>.s at Dry Central Thimble (DCT) of 3MW TRIGA Mark-II Research Reactor. In this study, the temperature at the particular points were calculated at the worst conditions following the 1/7<sup>th</sup> thumb rule of the total heat transferred by convection mechanism and also 120% of heat generation rates of  $\text{TeO}_2$  powder and quartz vial for conservative assessment of the Alcan material with assured safety. Finally the temperature at different locations of the quartz vial and necessary recommendations are made in order to safe irradiation of experimental samples at DCT of the reactor core with loading different quantities of  $\text{TeO}_2$  powder at different power levels of the reactor.

**Keywords:**  $\text{TeO}_2$  powder, One-dimensional analysis, DCT, Conservative assessment, Safe irradiation.

### 1. INTRODUCTION

Irradiation request (IR) from the Radio Isotope Production Division (RIPD) of Institute of Nuclear Science and Technology (INST) has submitted an IR to the Atomic Energy Research Establishment-Research Reactor Operation and Utilization Committee (AERE-RROUC) to irradiate 40 gm of  $\text{TeO}_2$  powder in a quartz vial with convex bottom at 3MW in the Dry Central Thimble (DCT). DCT is located in the central point of the reactor core, which is encircled in black color as shown in Fig.1. The thermal neutron flux at DCT is taken as  $8.71 \times 10^{13}$  n/cm<sup>2</sup>.s at 3MW. The geometry of the quartz vial is quite different from that of the old vials. It is very important to assess the temperature distribution of the quartz vial with 40 gm of  $\text{TeO}_2$  powder to ensure safe irradiation. The bottom surface of the old vial is concave upward where as the new vial is concave downward. It is observed that the contact area of the new vial is about 16 times higher than that of old one. The outer radius (1.15 cm) is also higher than that of old one (1.113 cm). Thickness of the new quartz vial is a little bit smaller than that of the old vial according to the data received from RIPD.

One-dimensional steady state axial heat conduction is considered to assess the temperature distribution in and around the  $\text{TeO}_2$  powder during its irradiation at 3MW (thermal) power level. Four different material layers namely; (i)  $\text{TeO}_2$  powder, (ii) Quartz vial, (iii) Al-Can

and (iv) DCT stopper plate are considered in the heat transfer path. The heat generated through nuclear fission reaction in  $\text{TeO}_2$  powder in the quartz vial is conducted through the quartz vial, through the aluminum can, and through the stopper plate to the coolant (water). The temperature of the water is presumed known to be about 60°C. It is assumed that 1/7<sup>th</sup> of the total heat is transferred through convection mechanism and the rest of the heat is transferred through conduction mechanism [1]. As Al-Can rests on the aluminum stopper plate and as its thermal conductivity is very high, it is assumed that significant amount of heat is dissipated through the axial (bottom) direction and fraction of the heat is transferred through the radial direction.

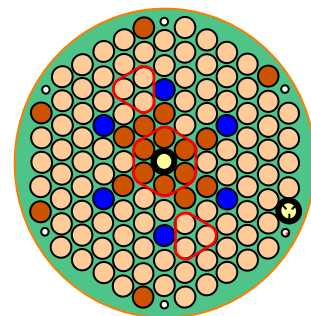


Fig 1: Reactor core configuration with DCT location at the centre of the core

Heat generation in  $\text{TeO}_2$  powder is mainly due to interaction of neutron ( $n$ ) and gamma ( $\gamma$ ) radiation. The value of heat generation rate for  $\text{TeO}_2$  powder during irradiation in the DCT is taken from reference [1]. For conservatism, total heat generation rate is taken to be 120 % higher than their actual values [Safety Factor (SF) =1.2]. Geometry factor was taken as 80% to simulate the real situation

## 2. METHOD OF CALCULATION OF TEMPERATURES

In order to calculate temperature at different locations, geometrical configuration is given in Figs .2 -3. Figures 2 and 3 show section views of the target material containment with DCT in the radial and axial directions, respectively. The thermo-physical properties of each material along with their figures are provided for convenience. Figure 4 shows the approximate contact area that plays an important role in transferring heat in the axial direction. Heat transfer mainly depends in the axial direction on surface contact area of the quartz vial on the Al-Can. Figures 5 and 6 show thermal resistances considered along the heat transfer path for two different approaches. In method-1, total heat transfer rate is considered. And In method-2, surface heat flux is considered. Both the methods show similar results. Centerline temperature of the  $\text{TeO}_2$  powder is determined using one-dimensional heat conduction equation with heat generation.

$t_4$  : thickness of air film between quartz vial and Al Can,  $t_4 = 0.1$  cm  
 $L$  : Length of quartz vial,  $L = 6.3$  cm

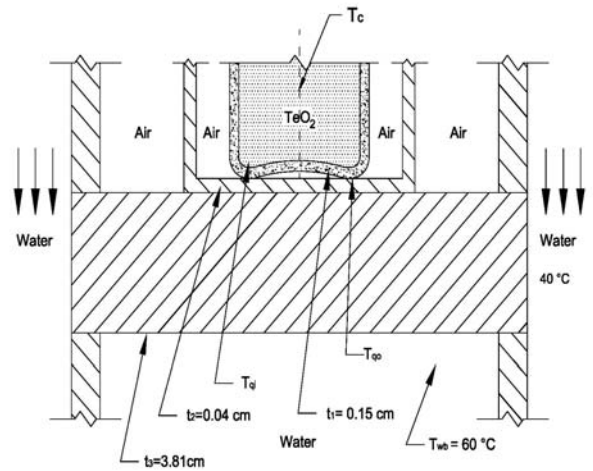


Fig 3: Section view (axial) of the target material containment with DCT

### (1) Physical Dimensions

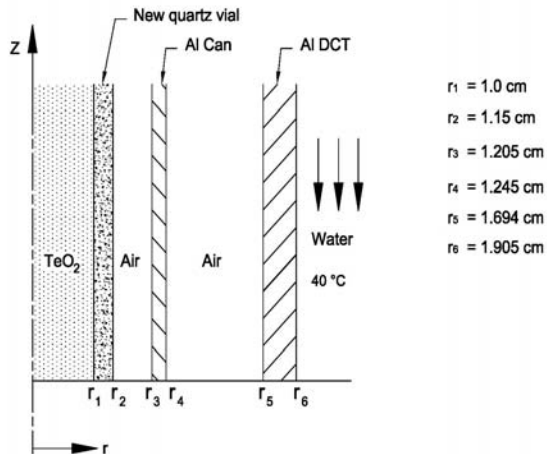


Fig 2: Section view (radial) of the target material containment with DCT

$r_1$  = inner radius of quartz vial,  $r_1 = 1.000$  cm  
 $r_2$  = outer radius of quartz vial,  $r_2 = 1.150$  cm  
 $r_3$  = inner radius of aluminum Can,  $r_3 = 1.205$  cm  
 $r_4$  : outer radius of aluminum Can,  $r_4 = 1.245$  cm  
 $r_5$  : inner radius of aluminum DCT,  $r_5 = 1.694$  cm  
 $r_6$  : outer radius of aluminum DCT,  $r_6 = 1.905$  cm  
 $t_1$  : thickness of quartz vial,  $t_1 = 0.15$  cm  
 $t_2$  : thickness of aluminum Can,  $t_2 = 0.04$  cm  
 $t_3$  : thickness of the stopper plate of aluminum DCT,  $t_3 = 3.81$  cm



Fig 4: Bottom contact area of quartz vial

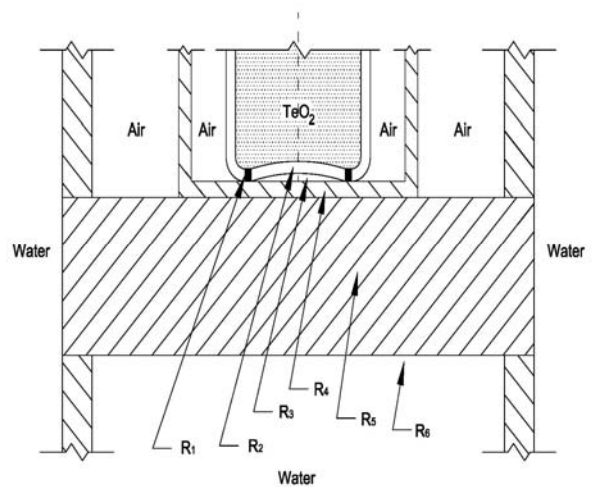


Fig 5 (a): Thermal resistances encountered during heat transfer from  $\text{TeO}_2$  powder in the axial direction

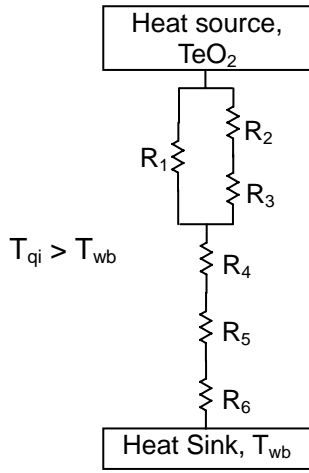


Fig 5(b): Circuit diagram of the thermal resistances along the heat transfer path

### Thermal Properties

#### (i) TeO<sub>2</sub> powder

$\rho_{Te}$  : density [2],  $\rho_{Te} = 4.5 \text{ g/cm}^3$   
 $h_{grTe}$  : heat generation rate (n+ $\gamma$ ) @  $5.56 \times 10^{13} \text{ n/cm}^2 \cdot \text{s}$ ,  $h_{grTe} = 1.664 \text{ W/g}$   
 $K_{Te}$  : thermal conductivity ,  $K_{Te} = 0.03 \text{ W/cm}^0\text{C}$   
 $m_{Te}$  : mass of TeO<sub>2</sub> in gram,  $m_{Te} = 40 \text{ g}$

#### (ii) Quartz vial

$h_{grqu}$  : heat generation rate (n+ $\gamma$ ) @  $5.56 \times 10^{13} \text{ n/cm}^2 \cdot \text{s}$ ,  $h_{grqu} = 0.008 \text{ W/g}$   
 $K_{qu}$  : thermal conductivity ,  $K_{qu} = 0.05 \text{ W/cm}^0\text{C}$   
 $\rho_{qu}$  : density,  $\rho_{qu} = 2.654 \text{ g/cm}^3$

#### (iii) Aluminum (Al 6061-T6)

$K_{al}$  : thermal conductivity,  $K_{al} = 2.3 \text{ W/cm}^0\text{C}$

#### (iv) Air

$K_{air}$  : thermal conductivity ,  $K_{air} = 0.00032 \text{ W/cm}^0\text{C}$

$P_{cf} = \frac{8.71 \times 10^{13}}{5.56 \times 10^{13}} [\text{TRF Flux} = 8.71 \times 10^{13} \text{ n/cm}^2 \cdot \text{s} @ 3\text{MW}]$

thermal Power.

$\therefore P_{cf} = 1.567$

$$Q_{Te} = m_{Te} \times h_{grTe} \times P_{cf} \times G_f \quad (1)$$

$$= 40 \times 1.664 \times 1.567 \times 0.8 \quad [G_f = 0.8]$$

$$= 83.44 \text{ W}$$

$$Q_{qu} = m_{qu} \times h_{grqu} \times P_{cf} \times G_f \quad (2)$$

$$= [\{\pi(r_2^2 - r_1^2) \times L + 2 \times \pi r_2^2 \times t_1\} \times \rho_{qu}] \times h_{grqu} \times P_{cf} \times G_f$$

$$= [\{\pi(1.15^2 - 1^2) \times 6.3 + 2 \times \pi \times 1.15^2 \times 0.15\} \times 2.654] \times 0.008 \times 1.567 \times 0.8$$

$$= 0.203 \text{ W}$$

$$Q_T = (Q_{Te} + Q_{qu}) \times SF \quad (3)$$

$$= [(83.44 + 0.203) \times 1.2] \text{ W} \quad [SF = 1.2]$$

$$= 100.37 \text{ W}$$

Since 1/7<sup>th</sup> of the total heat is transferred through convection mechanism and the rest of the heat is transferred through conduction mechanism, the total heat

conduction stands;

$$Q_{cond} = Q_T \times Q_{cf} \quad (4)$$

$$= 100.37 \times 0.857 \quad [Q_{cf} = 6/7 = 0.857]$$

$$= 86.02 \text{ W}$$

### 3) Contact areas in the Heat Transfer Path

Contact area of new quartz vial with Al Can,

$$A_1 = \pi \times (0.85^2 - 0.75^2) = 0.503 \text{ cm}^2$$

Area of trapped air under new quartz vial,

$$A_2 = \pi \times 0.75^2 = 1.767 \text{ cm}^2$$

Contact area of Al Can with aluminum DCT,

$$A_3 = \pi r_4^2 = \pi \times 1.245^2 = 4.87 \text{ cm}^2$$

Area under stopper plate of aluminum DCT,

$$A_4 = \pi r_5^2 = \pi \times 1.694^2 = 9.015 \text{ cm}^2$$

### (4) Thermal Resistances

$$R_1 = \frac{t_1}{K_{qu} A_1} = \frac{0.15}{0.05 \times 0.503} = 5.964 \text{ }^0\text{C/W}$$

$$R_2 = \frac{t_1}{K_{qu} A_2} = \frac{0.15}{0.05 \times 1.767} = 1.698 \text{ }^0\text{C/W}$$

$$R_3 = \frac{t_4}{K_{air} A_2} = \frac{0.1}{0.00032 \times 1.767} = 176.85 \text{ }^0\text{C/W}$$

$$R_4 = \frac{t_2}{K_{al} A_3} = \frac{0.04}{2.3 \times 4.87} = 0.0036 \text{ }^0\text{C/W}$$

$$R_5 = \frac{t_3}{K_{al} A_3} = \frac{3.81}{2.3 \times 4.87} = 0.34 \text{ }^0\text{C/W}$$

$$R_6 = \frac{1}{h_w A_4} = \frac{1}{4.5 \times 9.015} = 0.0247 \text{ }^0\text{C/W}$$

### 2.1 Temperature at Inside and Outside of the Quartz Vial (Method-1)

$$R_{eq(1)} = \frac{R_1 \times (R_2 + R_3)}{R_1 + R_2 + R_3}$$

$$\Rightarrow R_{eq(1)} = \frac{5.964 \times (1.698 + 176.85)}{5.964 + 1.698 + 176.85} \text{ }^0\text{C/W}$$

$$\therefore R_{eq(1)} = 5.7712 \text{ }^0\text{C/W}$$

$$R_{eq} = R_{eq(1)} + R_4 + R_5 + R_6$$

$$\Rightarrow R_{eq} = 5.7712 + 0.0036 + 0.34 + 0.0247 \text{ }^0\text{C/W}$$

$$\therefore R_{eq} = 6.1395 \text{ }^0\text{C/W}$$

$$Q_{cond} = \frac{T_{qi} - T_{wb}}{R_{eq}} \quad (5)$$

$$\Rightarrow T_{qi} = Q_{cond} \times R_{eq} + T_{wb} \quad (6)$$

$$= [86.02 \times 6.1395 + 60] \text{ }^0\text{C}$$

$$= [528.12 + 60] \text{ }^0\text{C}$$

$$\therefore T_{qi} = 588.12 \text{ }^0\text{C}$$

Again,

$$Q_{\text{cond}} = \frac{T_{\text{qi}} - T_{\text{qo}}}{R_{\text{eq}(l)}}$$

$$\Rightarrow T_{\text{qo}} = T_{\text{qi}} - Q_{\text{cond}} \times R_{\text{eq}(l)} \quad (7)$$

$$= [588.12 - 86.02 \times 5.7712] \text{ } ^\circ\text{C}$$

$$\therefore T_{\text{qo}} = 91.68 \text{ } ^\circ\text{C}$$

## 2.2 Determination of Centerline Temperature of TeO<sub>2</sub> Powder

One dimensional radial heat conduction equation with heat generation is;

$$\frac{1}{r} \frac{d}{dr} \left( r \frac{dT}{dr} \right) + \frac{\ddot{q}}{K_{\text{Te}}} = 0 \quad (8)$$

$$\Rightarrow \frac{d}{dr} \left( r \frac{dT}{dr} \right) + \frac{\ddot{q}r}{K_{\text{Te}}} = 0$$

$$\Rightarrow \frac{d}{dr} \left( r \frac{dT}{dr} \right) = - \frac{\ddot{q}r}{K_{\text{Te}}}$$

$$\Rightarrow r \frac{dT}{dr} = - \frac{\ddot{q}r^2}{2K_{\text{Te}}} + C_1 \quad (9)$$

$$\Rightarrow \frac{dT}{dr} = - \frac{\ddot{q}r}{2K_{\text{Te}}} + \frac{C_1}{r}$$

$$\Rightarrow T(r) = - \frac{\ddot{q}r^2}{4K_{\text{Te}}} + C_1 \ln r + C_2 \quad (10)$$

Applying boundary conditions;

$$\text{at } r = 0; \quad \frac{dT}{dr} = 0; \quad \text{from equation (5), } C_1 = 0$$

$$\text{at } r = r_1; T(r) = T_{\text{qi}}; \quad \text{from equation (6),}$$

$$T_{\text{qi}} = - \frac{\ddot{q}r_1^2}{4K_{\text{Te}}} + C_2$$

$$\Rightarrow C_2 = T_{\text{qi}} + \frac{\ddot{q}r_1^2}{4K_{\text{Te}}}$$

$\therefore$  From equation (6)

$$T(r) = - \frac{\ddot{q}r^2}{4K_{\text{Te}}} + \frac{\ddot{q}r_1^2}{4K_{\text{Te}}} + T_{\text{qi}}$$

The general heat conduction equation becomes;

$$\Rightarrow T(r) = \frac{\ddot{q}r_1^2}{4K_{\text{Te}}} \left[ 1 - \left( \frac{r}{r_1} \right)^2 \right] + T_{\text{qi}} \quad (11)$$

At  $r = 0$  in the general heat conduction equation, the centerline temperature of TeO<sub>2</sub> powder is

$$T_c = \frac{\ddot{q}r_1^2}{4K_{\text{Te}}} + T_{\text{qi}} \quad (12)$$

[Here,  $\ddot{q} = (h_{\text{grTe}} \times \text{pcf} \times \rho) \times \text{SF} \times G_f \text{ W/cm}^3$ ]

$$\Rightarrow T_c = \frac{1.664 \times 1.567 \times 4.5 \times 1.2 \times 0.8 \times 1^2}{4 \times 0.03} + 588.12$$

$$\Rightarrow T_c = (93.87 + 588.12) \text{ } ^\circ\text{C}$$

$$\Rightarrow T_c = 682 \text{ } ^\circ\text{C}$$

Table 1: Temperatures at different locations with varying conduction heat transfer rate in the axial direction [\* Equation number]

Q <sub>cond</sub> = 85.83 W	Heat Transfer through axial direction				
	100%	90%	80%	70%	60%
T <sub>c</sub> (°C) [12]*	682	629.18	576.37	523.55	470.74
T <sub>q</sub> (°C) [5]*	588.12	535.31	482.5	429.68	376.87
T <sub>qo</sub> (°C) [7]*	91.68	88.51	85.35	82.18	79

## 2.3 Temperature at Inside and Outside of the Quartz Vial (Method-2)

Volumetric Heat Generation:

$$\ddot{q}_{\text{Te}} = h_{\text{grTe}} \times P_{\text{cf}} \times \rho_{\text{Te}} \times \text{SF} \times G_f \times Q_{\text{cf}} = 1.664 \times 1.567 \times 4.5 \times 1.2 \times 0.8 \times 0.857 = 965 \text{ W/cm}^3$$

$$[\ddot{q}_{\text{qu}} = h_{\text{grqu}} \times P_{\text{cf}} \times \rho_{\text{qu}} \times \text{SF} \times G_f \times Q_{\text{cf}} = 0.008 \times 1.567 \times 265 \times 4.5 \times 1.2 \times 0.8 \times 0.857 = 0.027 \text{ W/cm}^3]$$

Heat Transfer Rate:

$$Q_T = V_{\text{Te}} \times \ddot{q}_{\text{Te}} + V_{\text{qu}} \times \ddot{q}_{\text{qu}} \quad (14)$$

$$\Rightarrow \frac{Q_T}{\pi \times r_2^2} = \frac{\Delta V_{\text{Te}} \times \ddot{q}_{\text{Te}} + \Delta V_{\text{qu}} \times \ddot{q}_{\text{qu}}}{\pi \times r_2^2}$$

$$\Rightarrow \ddot{q} = \frac{\Delta V_{\text{Te}} \times \ddot{q}_{\text{Te}} + \Delta V_{\text{qu}} \times \ddot{q}_{\text{qu}}}{\pi \times r_2^2}$$

$$\Rightarrow \ddot{q} = \frac{\frac{m_{\text{Te}}}{\rho_{\text{Te}}} \times \ddot{q}_{\text{Te}} + [\pi(r_2^2 - r_1^2) \times L + 2 \times \pi r_2^2 t_1] \times \ddot{q}_{\text{qu}}}{\pi \times r_2^2}$$

$$\Rightarrow \ddot{q} = \frac{40}{4.5} \times 9.65 + [\pi(1.15^2 - 1^2) \times 6.3 + 2 \times \pi \times 1.15^2 \times 0.15] \times 0.027}{\pi \times 1.15^2}$$

$$\Rightarrow \ddot{q} = \frac{87.78 + 0.21}{4.155}$$

$$\therefore \ddot{q} = 21.18 \text{ W/cm}^2$$

### 2.3.1 Thermal Resistances for Method-2

$$R'_1 = \frac{t_1}{K_{\text{qu}} \times \text{CF}} = \frac{0.15}{0.05 \times 0.16} = 18.75 \text{ cm}^2 \text{ } ^\circ\text{C/W}$$

$$R'_4 = \frac{t_2}{K_{\text{al}}} = \frac{0.04}{2.3} = 0.0174 \text{ cm}^2 \text{ } ^\circ\text{C/W}$$

$$R'_5 = \frac{t_3}{K_{al}} = \frac{3.81}{2.3} = 1.66 \text{ cm}^2 \text{ } ^\circ\text{C/W}$$

$$R'_6 = \frac{1}{h_w} = \frac{1}{4.5} = 0.222 \text{ cm}^2 \text{ } ^\circ\text{C/W}$$

$$R'_{eq} = R'_1 + R'_4 + R'_5 + R'_6$$

$$\Rightarrow R'_{eq} = 18.75 + 0.0174 + 1.66 + 0.222$$

$$\therefore R'_{eq} = 20.65 \text{ cm}^2 \text{ } ^\circ\text{C/W}$$

Again,

$$\ddot{q} = \frac{T'_{qi} - T_{wb}}{R'_{eq}} \quad (15)$$

$$\Rightarrow T'_{qi} = \ddot{q} \times R'_{eq} + T_{wb}$$

$$\Rightarrow T'_{qi} = 21.18 \times 20.65 + 60$$

$$\therefore T'_{qi} = 497.37 \text{ } ^\circ\text{C}$$

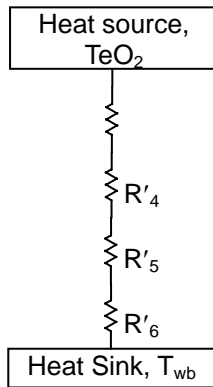


Fig 6: Circuit diagram of the thermal resistances along the heat transfer path

### 3. CONCLUDING REMARKS

Based on the calculation results, it is found that temperature of the inner surface of the quartz vial ( $T'_{qi}$ ) is found at 497.37  $^\circ\text{C}$  using method-2. This temperature agrees well with the temperature calculated by method-1, which is about 80 % heat generated (Ref.:Table 1) in the  $\text{TeO}_2$  powder transferred by conduction mechanism through the axial (bottom) direction. There is a small temperature difference ( $T_{qi}$  &  $T'_{qi}$ ;  $\cong 15 \text{ } ^\circ\text{C}$ ) of the inner surface of the quartz vial between the two methods, which can be accepted within a small range of uncertainty. The outer surface temperature of the quartz vial ( $T_{qo}$ ) is found to be 85.35 $^\circ\text{C}$ . The estimation of surface temperatures is calculated for a quartz vial containing 40 gm of  $\text{TeO}_2$  powder during its irradiation in the DCT at 3MW thermal power level. From these calculative results, it can be seen that there is a very high temperature gradient between the inner and outer surface of the quartz vial. Such a high temperature gradient may not be a problem for causing excessive thermal stress in the quartz vial.

It is also found from the calculation that the centerline temperature of the  $\text{TeO}_2$  powder ( $T_c$ ) is 576.37  $^\circ\text{C}$ , which

is below the sintering temperature of the  $\text{TeO}_2$  powder. The above-mentioned temperatures are found based on the conservative values of heat generation rate, contact areas and geometry factor.

### 4. RECOMMENDATIONS

The problem is a complicated one. One-dimensional equations are used for simplicity. 2 or 3-dimensional analysis (numerical) may be used for better results. However, as a first approximation, one-dimensional heat transfer analysis is very much useful to assess the temperature. Commercial temperature indicators (color code)/thermocouples can be inserted at inner and outer surfaces of the quartz vial to verify the calculated results with the experimental one.

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### 6. NOMENCLATURE

A	: Heat transfer area ( $\text{m}^2$ )
C	: Constant parameter
CF	: Contact factor
$G_f$	: Geometry correction factor
$h_{gr}$	: Heat generation rate (W/g)
$h_w$	: Convective heat transfer coefficient of water under the stopper plate of aluminum DCT, $\text{W}/\text{cm}^2 \text{ } ^\circ\text{C}$
K	: Thermal conductivity (W/m K)
M	: Mass of $\text{TeO}_2$ powder
$P_{cf}$	: Correction factor for power
$Q_{cf}$	: Heat conduction factor
$Q_{Te}$	: Heat from $\text{TeO}_2$ powder, W
$Q_{qu}$	: Heat from quartz vial, W
$Q_T$	: Total heat generated ( $Q_{Te}+Q_{qu}$ ), W
$Q_{cond}$	: Total heat transferred through conduction mechanism, W

$\ddot{q}_{Te}$  = Volumetric heat generation of  $TeO_2$  powder,  $W/cm^3$   
 $\ddot{q}_{qu}$  = Volumetric heat generation of quartz vial,  $W/cm^3$   
 $\dot{q}$  = Heat flux in axial direction,  $W/cm^2$   
 $r$  : Local radius  
 $R$  : Thermal resistances (Method-1),  $^{\circ}C/W$   
 $R'$  : Thermal resistances (Method-2),  $cm^2.^{\circ}C/W$   
 $R_{eq(1)}$  : Equivalent resistance of  $R_1$ ,  $R_2$  and  $R_3$   
(Method-1),  $^{\circ}C/W$   
 $R_{eq}$  : Equivalent resistance (Method-1),  $^{\circ}C/W$   
 $R'_{eq}$  : Equivalent resistance (Method-2),  $cm^2.^{\circ}C/W$   
 $SF$  : Safety factor  
 $T_{wb}$  : Water temperature under the stopper plate of  
aluminum DCT,  $^{\circ}C$   
 $T_{qi}$  : Inner temp. of the quartz vial (Method-1),  $^{\circ}C$   
 $T'_{qi}$  : Inner temp. of the quartz vial (Method-2),  $^{\circ}C$   
 $T_{qo}$  : Outer temperature of the quartz vial,  $^{\circ}C$   
 $T_c$  : Center temperature of the  $TeO_2$  powder,  $^{\circ}C$   
 $\rho$  : Density ( $kg/m^3$ )